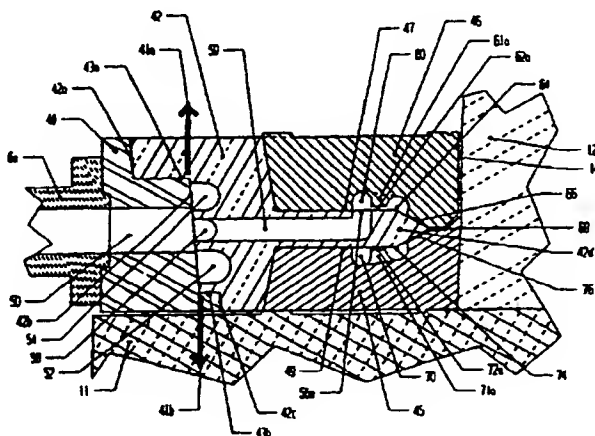




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(54) Title: REGULAR DIVISION OF MELT FLOW IN EXTRUSION OF BLOWN FILMS



(57) Abstract

An extrusion die having a plurality of die layers stacked one upon the other in a direction generally parallel to the central axis. Each of the layers has an annular flow distribution ring (40) having an outer generally cylindrical surface and an annular feed ring surrounding and engaging the outer surface of the distribution ring (42, 42d). At the engaged surfaces of the feed and distribution ring, the flow from the feed ring is divided into a number of substantially equal flow portions. Seals (43a, 43b) between adjacent engaged surfaces confine the flow between the circumferential surfaces of the feed and distribution ring. Half of the flow portions are directed to a recombination region (45, 46) on one side of the distribution ring (42d), and half are directed to a recombination region (45, 46) on the other side of the ring (42d). In recombining, weld lines are formed in high flow areas minimizing the deleterious effect of polymer degradation. Subsequently, the flows on the opposite sides of the distribution ring (42d) are recombined such that the weld lines from one half are first modified to exhibit lower flow and then are layered with non-weld line portions modified to exhibit higher flow from the other half. This further minimizes the negative effect of weld line areas. Flow from the two sides is regularly divided to yield even distribution of the combined flows.

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REGULAR DIVISION OF MELT FLOW IN EXTRUSION OF BLOWN FILMS

Field of the Invention

The present invention relates to improving the quality of extruded annular products, particularly products produced by plastic resin extrusion lines and most particularly blown plastic film.

Background of the Invention

In making such cylindrical products, the material from which the product is formed is extruded from an annular extrusion die and pulled along the die axis. In the case of blown film, plastic resin is extruded from a heated extruder having an annular die and the molten polymer is pulled away along the die axis in the form of an expanded bubble.

After the resin cools to a set diameter as a result of application of cooling air, the bubble is collapsed and passes into nip rolls for further manufacturing steps.

As the film is extruded, thickness variations occur about the circumference of the bubble. The presence of thickness variations creates problems for downstream conversion equipment such as printing presses, laminators, or bag machines. In processes where the film is not converted in-line, but is wound onto a roll prior to converting, the thicker and thinner areas of many layers on the roll create hills and valleys on the roll surface which deform the film and magnify the subsequent converting problems especially with larger diameter rolls. It

is therefore desirable to minimize such thickness variations, not only in blown film but in other extruded cylindrical products as well. To achieve this goal, processors use expensive equipment designed to randomize the position of these thick and thin areas over time or to automatically reduce the magnitude of these variations so that the finished roll is suitable for later converting steps.

It is recognized that thickness variations are caused by a variety of factors such as circumferential nonuniformity in flow distribution channels (ports and spirals) within the die, melt viscosity nonuniformity, and inconsistent annular die gaps through which the polymer exits the die. Flow distribution problems inside the die are of particular concern because they typically take the form of relatively sharp, closely spaced high and low spots which are commonly referred to as "port lines". Additionally, variability of the cooling air and nonuniformity of air aspirated into the cooling air stream from the atmosphere surrounding the extrusion line are major contributors to film thickness variation. Many film processors rely on conventional blown film equipment to determine the film thickness. This approach typically yields an average variation of +/- 10 to 20% in film thickness overall, with the largest contributor typically being that of port lines.

It is desired to make improvements in the die to obtain higher quality film and other products so that the downstream equipment can be run faster and longer and so that the end use products will have more
5 consistent thickness.

One major difficulty to overcome in designing a die is how to uniformly convert a typically non-uniform flow of molten polymer or other material that is conveyed to the die via a "melt" pipe into a
10 relatively thin annular flow. Annular flow implies that there is an inner and outer forming wall as opposed to just an outer enclosing wall such as exists with the melt pipe. To introduce this inner forming wall into
15 the molten stream requires that this new inner forming wall be rigidly fixed within the cavity of the outer enclosing wall of the die. To do this, connecting structures must be placed within the flow path of the molten material that temporarily disrupt the flow forming multiple,
20 separate flows which then pass by the connecting structures and must be recombined in some way. Unfortunately, molten polymer exhibits non-uniform melt viscosity due mainly to variations in molecular level
25 properties as well as local polymer temperature. These viscosity effects are collectively referred to as the rheology. One such property of major concern is that polymers exhibit "non-Newtonian" flow behavior. This means that the viscosity of the polymer changes depending on how fast

it is moving through a given channel. The net effect when all viscosity effects are combined is that the polymer tends to segregate by viscosity making uniform recombination of multiple polymer flows very difficult. 5 Additionally, molten polymer remembers its previous flow history and instead of seamlessly recombining, the multiple polymer flows tend to form unwanted "weld lines" where adjacent flows are recombined. The 10 problem of weld lines intensifies when degradation of the polymer occurs due to low polymer flow rates.

Several approaches are presently employed to provide for connecting structure between the outer and inner forming walls of the 15 die. One approach feeds from the centerline axis, a small distribution chamber in the die. This chamber separates and directs the polymer into several smaller, equally spaced pipes called ports, which diverge radially at some angle to the flow axis of the incoming melt. These ports 20 convey the polymer out to a diameter appropriate for recombining into the annular flow which will exit the die. Another approach creates a mushroom shaped distribution chamber out of which relatively small, 25 highly streamlined, spider-like connecting structures diverge radially at an angle to the flow axis that allow for quick recombination before forming the generally axial annular flow that exits the die. Yet another approach feeds the die radially from the side of the die and divides the

flow one or more times through a network of flow channels similar to the branches of a tree which ultimately convey the separate polymer streams to a diameter appropriate for recombining into the annular flow which will exit the die. Generally, one or more of the methods of flow separation must be employed in a blown film die, but each causes problems with segregation and potential for weld lines to form. Special recombination techniques must be employed to limit these effects.

Several techniques are used to recombine individual molten material flows into the annular flow that exits from the die. Some are designed to overlap the separate flows creating an onion-like layering effect while others simply butt opposed flows up against each other and allow time, temperature and pressure to force recombination to occur.

In blown film production, the most common recombination technique commercially available employs channels which spiral around the axis of the die. These so-called spirals, overlap one another and allow molten polymer to gradually bleed out of the channel over a "land", eventually to flow toward the annular exit of the die forming a layered, almost onion-like recombination flow. This annular flow of polymer exits the die at what is commonly referred to as the die lip. The major problem with this approach is that the flow channels and lands must be made non-uniform to compensate for Non-Newtonian

flow and other nonuniformities exhibited by the polymer.

Unfortunately, major differences exist in the flow characteristics of various polymer materials that are processed. For a given die design, it may be possible to obtain even distribution around the flow annulus for one material, however it will not be even for others. Instead, other materials tend to form somewhat sinusoidal high and low flow spots in locations which depend on the material properties being processed. Thus the spiral design approach is limited in its capability to process a broad range of materials while simultaneously holding thickness variations to a consistent, predictable minimum.

A further problem is that the polymer or other material must necessarily take a long period of time to flow through the passages, i.e., a high residence time, which can lead to degradation of the material. Additionally, as the material flows through each passage, significant backpressure is created.

In "pancake" designs which incorporate distribution channels and the spirals substantially into the face of a plate that is coaxial with the flow axis of the die, the wetted surface area is quite large so that, when combined with higher pressures, resulting separation forces between adjacent plates can grow to be so large that the die cannot be held together. This forces the designer of such dies to limit the pressure

magnitude which tends to degrade even distribution. Further, in many cases, lower pressure is attained by enlarging the flow passages; however this leads to higher residence time causing degradation of polymer properties. In practice, pressure and distribution effectiveness must be balanced which can lead to limitations on how large the die can be.

A less commonly used recombination approach does not overlap the flows but instead joins them at one or more discrete locations. In these locations where two opposed flows join together, the flow is very low causing the material to have very long residence times which degrades the polymer. This degraded polymer forms a distinct weld line that exhibits poor optical properties and reduced strength which have tended to limit the use of these designs. On the other hand, since there is no overlap, the flow channels are shorter than in overlap designs. This provides benefits in lower pressure and residence time which limits degradation and allows for larger designs. Non-overlapping designs also benefit from the clearly defined flow paths which force the polymer through the same geometry regardless of melt flow characteristics as opposed to the shifting around of the flow path associated with overlapping designs. This simplifies the die design process since non-Newtonian flow is well understood through defined geometries.

Unfortunately, non-uniformities in distribution still occur as the melt flow characteristics change from those that were used to design the die.

5 As a wider range of polymer choices are made available, this becomes more of a problem.

Processors are presented with a growing number of choices of extrusion materials, each with their own special properties. For
10 example, some polymers resist water vapor, others resist oxygen penetration, still others provide high strength or resist puncture. Increasingly, processors are finding innovative uses for these materials, oftentimes finding it desirable to combine different polymers together in
15 a layered or "coextruded" structure to yield property benefits in several areas. To do this, dies are designed with multiple entry points which distribute the polymer flow into separate annular flows and subsequently layer these flows one inside the other while still inside the die.
20 Although non-overlapping designs have been used, most prevalent are overlapping designs either in a concentric or pancake configuration. Pancake designs are better suited to larger number of layers because the
25 individual layers can be stacked one on top of each other. Concentric designs are limited to about 5 to 7 layers simply because the die grows so large in diameter as to become impracticable.

It has long been recognized that having multiple layers can provide a secondary benefit in that thickness variations present in each layer can somewhat offset one another. This has a drawback; since each layer's variation depends on associated melt flow properties, throughput rate, temperature etc., the variations typically will not always average out. In fact, they can even align one on top of each other yielding no thickness averaging whatever. This is especially true of overlapping designs since the melt variations shift significantly in position and magnitude with even subtle changes in a given layer. Commercial coextrusion dies are designed with adjacent layer spirals that typically wrap in opposed directions in an effort to capitalize on this averaging effect. In the case of concentric die designs, the spirals for each layer are necessarily different in design because they do not spiral around at the same distance from the flow axis of the die. Pancake designs can be designed with the same mechanical geometry, however the path length to the die lip is necessarily different for each layer because they are stacked one on top of each other. This causes differences in the flow behavior since each layer operates at a different pressure. It has been observed that commercially available dies designed to capitalize on averaging effects exhibit both very good and very bad variation in total thickness as the throughput rate is raised through its full operating

range. This occurs as resultant layer variations first oppose (good) then align (bad) with one another. An additional problem with these designs is that even if thickness variations are opposed, yielding good overall variation, the individual layer distribution can still be bad. This has a negative effect, especially when each layer is designed to take advantage of different film properties - the layers responsible for providing a barrier to oxygen and separately to water vapor can individually be highly variable even though the total thickness is uniform. It is highly desirable to achieve uniform distribution for each individual layer as well as for the combination of multiple layers.

Summary of the Invention

The present invention features a regular division (RD) die which provides uniform distribution of molten extrusion material to each individual layer and exhibits a high degree of insensitivity to melt flow properties and a pressure resistive distribution system that does not limit the size of the die. This die design has particular application to the extrusion of polymeric blown film, but also applies to other forms of extrusion requiring an annular die. Blown film extrusion lines typically include a heated extruder for melting and pressurizing a flow of molten plastic resin, an annular die through which the molten resin extrudes and

from which it is pulled away along an axis in the form of an expanding bubble, and an air cooling device constructed to direct cooling air into cooling contact with the bubble, to flow along the bubble and cause the molten resin to cool as the film expands until substantially fixed maximum bubble diameter is achieved at a frost line spaced from the annular die.

The RD design may be included as an integral part of one or more individual die layers within the complete die. According to one preferred embodiment, the RD design is integrated separately in each layer of a pancake style stackable die. Each layer includes a series of concentric rings one inside of the other that performs the functions of feeding, distribution and recombination. These rings surround and contact one another to allow the polymer to pass between them unimpeded through passages cut into the surfaces of and/or through them. The rings are bolted together forming a single unitized layer that is stacked face to face with the other layers of the complete die, each layer with its central geometrical axis being coaxial with the flow axis of the die. Polymer is separately fed into the outside diameter of the outer feed ring of each layer, the polymer passing straight radially through the feed ring wall to the radially interior associated distribution

ring. For purposes of the ensuing discussion, the location of the input through the feed ring is at location 0°.

5 The distribution ring has flow channels machined into its radially outwardly-facing surface which act to divide the flow one or more times. Cutting the channels into the outside surface (or alternatively, the radially inwardly facing surface or both) eliminates the detrimental
10 effects of separation forces caused by polymer pressure: the forces produced by the polymer act against the surrounding feed ring instead of on the bolts which hold the layer(s) together.

 In the distribution ring, the polymer flow input from the feed
15 ring is divided into an even number (2^n) of separate and equal flows. In the preferred embodiment, the input flow is divided into eight (2^3) flows, in three stages. The first division of flow occurs at 0°, at which point the polymer flow is divided in two and each half is directed into
20 one of two channels, each of which wraps 90 degrees around the circumference of the ring, one clockwise from 0 degrees to 90 degrees and the other counter-clockwise from 0 degrees to 270 degrees. At the
25 90 and 270 degree points, each flow (half of the original) turns and travels axially for a short distance prior to being divided a second time. The second divisions occur separately at the 90° and 270° points; at each of which the flow is again divided in half and the resulting portion

of the flow (one quarter of the total input flow) directed into one of a pair of channels which wrap 45° in opposite directions from, respectively, the 90° and 270° points, around the outside of the ring.

5 These four flows end up at, 45°, 135°, 225° and 315°; at which points the flow is divided again, this time into opposite wrap angles of 22.5. The end result of these three divisions is eight separate flows which end

10 at 45 degree intervals at, respectively, at 22.5°, 67.5°, 112.5°, ... , 337.5. It will be noted that, after each division, equal opposite wrap angles ensure that there is equal path length and thus equal pressure drop for any path through which the polymer might flow.

15 Each of these eight divided flows then passes radially inwardly through the first distribution ring, either directly to the recombination rings or, if further division is desired, to a second distribution ring. It will be recognized that, by using more than one distribution ring, a

20 larger number "n" of divisions can be accomplished without pressure penalties. In any event, after the desired number of divisions are made in the distribution rings, the resulting flows are conveyed radially

25 inwardly to the recombination rings through a divider plate that forms an integral part of the final (e.g., the most radially inward) distribution ring.

The divider plate is relatively thin (measured axially of the die) compared to the main body of the distribution ring of which it is a part.

5 The divider plate extends inwardly from the portion of the final radially inward distribution ring that forms the 2ⁿ polymer flows and tapers to a thin edge at its inner circumference. Within the divider plate, and generally prior to the taper, the 2ⁿ radial flows are alternately diverted to one side of the plate or the other. This provides two separate but identical flow patterns, each of which includes $2^{(n-1)}$ recombination flows, issuing from ports located in either the upper or the lower face of the divider plate. These flows in turn are fed to a pair of recombination
10 plates that abut the upper and lower faces of the divider plate.

One recombination plate is mounted on either side of the tapered portion of the divider plate. The recombination flow ports on one side of the divider plate are offset in such a way as to be centered between
20 ports on the opposite side of the divider plate. This allows for precise, mirror image recombination to take place, "split" on opposite sides of the divider plate. These split, mirror-imaged flows join together at the inner edge of the divider plate. The recombination flow channels on
25 each side of the divider plate are designed to create a flow distribution that, when added to its mirror image, results in a flat flow profile.

Insensitivity to melt rheology is attained by forcing the recombination plate flow to distribute in a non-overlapping manner, thus yielding predictable, non-shifting resultant polymer flow. Weld lines are avoided by placing an interceding land area directly in front of each port with the main flow channel passing on a diameter behind the land. Thus some of the flow from each port passes over the land and, of what remains, half flows down the channel one way and the other half flows in the opposite direction. Eventually the channel flow from one port meets opposite direction flow from the adjacent port. At this point, the main flow channel passes radially inward between the ends of adjacent lands. This creates a weld area, but because the weld area is in a high flow region the problem of polymer degradation is substantially eliminated. The main flow channel then splits again and passes on a diameter in front of each of the associated lands such that half flows down the channel one way and the other half goes the opposite direction. Thus the flow which originally was diverted around the land via the main flow channels is recombined with the land flow in a way which is predictably stable but yields a layered effect, similar to that produced in a spiral design but without shifts in position. The now annular and radially inwardly directed recombination flow passes over a final land to the tip of the divider plate where its mirror imaged split

flow from the opposite side of the divider plate is added. The final channel and land are cut in such a way as to insure a smaller flow where the high flow weld line occurs and a larger flow centered on the interceding land. Upon addition of its mirror image, the deleterious effects of the weld area is minimized by the addition of the mirror images larger (non-weld) flow area.

The shape of the flow issuing from the recombination area on each side of the divider plate prior to the flows being recombined is important to achieving a combined uniform flow from opposite sides of the divider plate. Although for a given material, the individual flows from each halve may also be uniform, they do not necessarily have to be. Rather, there is a wide diversity of curves which can be programmed into the design of the flow channels which after addition yield a uniformly flat combined profile. The mathematical study of "regular divisions of the plane" such as used in the study of crystallography or as can be found in graphical representations by M.C. Escher depict many suitable examples of both simple and complex profiles. A preferred profile for each split flow, is a straight line "triangle" profile which linearly increases from a minimum flow at the high flow weld to a maximum in line with the port. This profile repeats itself without discontinuity around the diameter of the layer. A second

preferred split flow profile is a "sinusoidal" profile which also has its minimum at the high flow weld and maximum in line with the port.

5

Brief Description of the Drawings

Figure 1 is a schematic side view showing a blown film extrusion apparatus which includes a multi-layer regular division die according to the present invention.

10

Figure 2 is a schematic cross section (taken at A-A of Figure 3) side view on an enlarged scale of the blown film extrusion regular division die of Fig. 1.

15

Figure 3 is a plan view of the general arrangement for a typical multi-layer blown film extrusion die.

20

Figure 4 is a partial cross sectional side view (taken at B-B of Figure 4a) of one layer for the regular division die showing the general locations of the feed inlet, dividing channels, recombination ports and channels.

25

Figure 4a is a plan view of one layer of the regular division die of Figure 1, showing the general locations of the feed inlet, dividing channels, recombination ports and channels.

Figure 4b is a schematic illustration, centered on the bore of the feed inlet of one layer of the regular division die of Figure 1, showing the general locations of the feed inlet, dividing channels, recombination ports and channels on the exterior surface of the layer, as viewed looking radially inwardly.

Figure 5 is a schematic illustration of an upper recombination channel and associated land area, as viewed looking upwardly from the upper surface of the tapered portion of the distribution plate.

Figure 5a is a schematic illustration of a lower recombination channel and land area as positioned relative to Figure 5, viewed looking downwardly from the lower surface of the tapered portion of the divider plate.

Figures 6 and 6a are schematics cross sections of typically desirable flow proportions from upper and lower recombination rings.

Description of the Preferred Embodiments

Figure 1 illustrates a blown film extrusion system in which molten plastic resin is extruded to form blown film. Except for the die 10, the system of Figure 1 and its operation are generally conventional. In general, plastic pellets are fed into a feed hopper 2a and are transferred into an extruder 4a where they are melted, mixed and pressurized by the action of an extruder screw. The melt exits extruder

4a and is conveyed through melt pipe 6a where it is directed into blown
film die 10. Die 10 is designed to form the melt into an annular,
5 cylindrical plastic melt flow 14 which is then extruded from an annular
orifice die lip 16 at the top of die 10. This annular melt flow is
continually drawn away from the annular die lip 16 in a manner
generally concentric with a process centerline 18. The annular diameter
10 of the melt flow enlarges as it progresses from the die until it reaches
frost line 20 (indicated diagrammatically by a saw-tooth line) to form a
cooled, solidified plastic tubular film bubble 22.

Primary cooling air for the process is supplied to external air
15 ring 24 from a conventional air source (not shown). The air is applied
to contact the extruding plastic melt adjacent the base portion of the
bubble by air ring lips 26. The air flows in annular air streams 28 along
the outside expanding surface of the bubble. On some blown film
20 processes, other forms of cooling are also employed. One such system
(not shown) applies cooling air to the inside surface of the bubble,
according to known techniques, and is commonly referred to as internal
bubble cooling, or just "IBC". The plastic melt is cooled sufficiently to
25 solidify into tubular bubble 22 at frost line 20.

Also according to known techniques, tubular bubble 22 is
continually drawn upward through collapsing frame 150, 150a where it

is compressed into a flat sheet of film 22a, also known as "layflat," as it passes through a nipping point between nip rolls 152 and 152a. These nip rolls are driven to continually pull the film through the extrusion process. Layflat film sheet 22a is then converted and/or wound into finished product by downstream processing equipment such as winder 156.

Figure 2 shows a schematic cross section side view of the blown film extrusion die 10 of the regular division type with multiple die layers 30a, 30b and 30c. Die layers 30a, 30b and 30c are essentially identical, and are rotated relative to each other as shown in Figure 3. Each layer converts melt feeding in from a respective melt pipe 6 to cylindrical plastic melt flow 14 which is conveyed toward die lip 16 around a cylindrical inner mandrel 12. Thus, layer 30a converts melt flow from melt pipe 6a to melt flow 14a, layer 30b forms a second cylindrical plastic melt flow 14b which is conveyed toward die lip 16 around cylindrical plastic melt flow 14a and inner mandrel 12, and layer 30c forms a third cylindrical plastic melt flow 14c which is conveyed toward die lip 16 around cylindrical plastic melt flows 14b and 14a, and inner mandrel 12. The three cylindrical plastic melt flows 14a, 14b and 14c layer adjacent to each other, and thus make up the total cylindrical plastic melt flow 14 which flows between inner mandrel 12 and outer

mandrel 15 until it exits through annular die lip 16. Layer 30a is held to die base 11 by a multiple bolts 34a. Layer 30b is stacked on top of and held to layer 30a by multiple bolts 34b. Layer 30c is stacked on top of and held to layer 30b by multiple bolts 34c. At the top of the stack, outer mandrel 15 is stacked on top of and held to layer 30c by a multiple bolts 34d. O-ring seals in annular seal areas 32, 32a, 32b, and 32c prevent plastic melt from flowing outward between the respective flat, axially-facing, abutting surfaces formed by die base 11, layers 30a, 30b, 30c and mandrel lip 15.

Figure 3 shows a plan view of the general arrangement for a typical blown film extrusion die 10 of the regular division type with multiple layers such as 30a, 30b and 30c of Figure 2. As shown in Figure 3, layer 30a is fed from extruder 4a by melt pipe 6a. Layer 30b and associated extruder 4b and melt pipe 6b are positioned at an angle to layer 30a and associated extruder 4a and melt pipe 6a. Similarly, layer 30c and associated extruder 4c and melt pipe 6c are positioned at an angle to layer 30b and associated extruder 4b and melt pipe 6b. This angle, e.g., about 60 degrees, is chosen to be large enough to provide clearance between adjacent extruders and melt pipes. Annular die lip 16 is formed by the outside surface of inner mandrel 12 and the inside surface of outer mandrel 15. Multiple bolts 34d are arranged to hold

outer mandrel in place. Multiple bolts 34b, shown on Figure 2, are directly beneath multiple bolts 34d. Multiple bolts 34a and 34c, also shown on Figure 2, are one above each other and positioned in between stacked multiple bolts 34b and 34d so as not to interfere with one another. Any number of layers can be accommodated by this approach simply by stacking and bolting them in place as demonstrated in Figures 2 and 3.

Figure 4 is an enlarged cross-sectional view of a portion of the die 10 of Figure 1 that includes layer 30a, and Figure 4a is a top plan view. Layer 30a is composed of a series of concentric rings (feed ring 40, distribution ring 42 and recombination rings 45, 46) one inside of the other, that perform the functions of feeding, distribution, and then recombining the flow of molten extruded material. In the illustrated embodiment, plastic and polymer flow passes radially through feed passage 50 to the outside diameter of distribution ring 42.

Feed ring 40, as shown most clearly in Figures 4 and 4a is annular and has a generally vertical surface to which melt pipe 6a is attached, and a feed passage extending radially through it to a stepped inner surface that engages the outer radially directed surface of annular distribution ring 42.

Distribution ring 42, in turn, defines a outer radially-facing surface that forms a series of annular steps 42a, 42b, 42c, each of which has a generally vertical (but slightly sloped) radially-facing wall, and which in this embodiment are separated by flat, parallel (to each other and perpendicular to the axis of the die and layer) annular surfaces. The underside of the top, largest diameter wall portion 42a and the underside of the middle diameter wall portion 42b, seal against corresponding surfaces formed at the inner radial diameter of feed ring 40. The O-rings 43a and 43b provide seals at the abutting surfaces, and bolts 44 (see Figure 2) hold the distribution ring and feed ring tightly together.

At its interior side, distribution ring 42 includes an annular divider plate portion 42d, centered on the overall height of the distribution ring but itself having a vertical height (measured along the axis of the distribution ring and die) that is not more than about 20% that of the overall distribution ring 42. As shown most clearly in Figure 4, in the illustrated embodiment, the top and bottom surfaces of divider plate portion 42d are flat and parallel to each other throughout most of the radial width of the divider plate portion, but taper towards each other adjacent the divider plate portion's inner edge.

Recombination rings 45 and 46 overlie the top and bottom of divider plate portion 42d, and are bolted together by bolts 34. Adjacent

their radially inner edges, recombination rings extend radially inwardly of the inner radial edge of divider plate portion, are closely adjacent to each other, and terminate close to the outer surface of inner mandrel 12.

5 The principal function of distribution ring 42 is to divide the single flow from feed ring 50 into a number (i.e., 2^2 in the preferred embodiment 2^3 , i.e., 8) identical flow portions. To accomplish this, a series of flow division channels 52, 54 and 58 are machined into the outer, generally vertical radially facing surface of step 42b. The size and/or quantity of division channels (channels 52, 54 and 58 are shown in the illustrated embodiment) are limited only by the vertical dimension of the outside diameter of distribution ring 42. Flow division channels 10 52, 54 and 58 divide the melt from feed passage 50 of feed ring 40 into eight separate radial port flows 59. Because most of the flow is between the radially-facing surfaces of the feed ring 40 and distribution ring 42, it will be evident that the forces 41a and 41b, along the die axis, which tend to move the distribution ring 42 and feed ring 40 apart are relatively small since they act only on the projected area (from a plan view) between seals 43a and 43b.

15 20 25 The arrangement of the division channels is shown most clearly in Figure 4b, which is a fold out (or unwrapped) schematic illustrating the radially-outward facing surface of wall portion 42b of division ring

42. As shown, division channels 52, 54 and 58 all extend circumferentially around the outward facing surface of the division ring, and lie generally perpendicular to the axis of the die. Flow from inlet feed passage 50 passes downwardly (through a short channel 51 extending parallel to the die axis and generally perpendicular to division channel 52, into the center of division channel. Channel 52 wraps a total of 180 degrees around the exterior of distribution ring 42, 90 degrees in opposite directions from the point at which the flow from inlet 50 is introduced into channel 52, and separates the melt flow from inlet 50 into two oppositely directed flows. At each of the ends of channel 52, a short vertical channel 53 directs the flow in the respective half of channel 52 (axially of the die layer) into the center of a respective one of flow channels 54. Division channels 54 each wrap a total of 90 degrees (45 degrees in each direction from the point at which flow from a channel 53 is directed into the respective channel 54) around the exterior of distribution ring 42, and divides the melt flow from channels 52 into a total of four flows. At each end of each division channel 54, each respective flow portion is again directed vertically a short distance, through a short channel 55, into the center of a respective one of division channels 58. Division channels 58 each wrap 45 degrees (22.5 degrees in opposite directions from the point at

which flow from channel 55 is directed into the respective division
channel 58) around the outside of distribution ring 42) and again divide
the flow, this time into a total of eight equal flow portions. At each end
of each of distribution channels, the respective flow portion is directed
into one of eight radial channels 57, 59, which convey the flow portion
radially through distribution ring 42 to (as shown in Figures 2 and 4)
either the upper (in the case of channels 59a, b, c, d) or the lower (in
the case of channel) 59a', b', c', d') surface of divider plate portion of the
distribution ring. As shown, each radial channel 59', extends radially
inwardly from a respective one of division channels 58 to the respective
surface of divider plate portion 42d, at a point just radially outwardly of
the tapered portion of the divider plate portion. The polymer melt flow
from division channels 58 is equally split to the top and bottom of the
divider plate portion; half goes to upper ports 56a, 56b, 56c and 56d and
the other half to lower ports 57a, 57b, 57c and 57d.

It will be noted that all of flow passages 50, 52, 54, 58, 59 of
distribution plate 42 are symmetrical such that the path length that melt
must travel to reach each port is equal, ensuring even distribution.

At recombination rings 46 upper ports 56a, 56b, 56c and 56d on
the upper side of divider plate 42d evenly distribute their associated
melt flow to four equally spaced positions between the upper side of the

divider plate and upper recombination ring 46. At ring 45 lower ports
57a, 57b, 57c and 57d evenly distribute their melt flow to four equally
5 spaced positions between the lower side of the divider plate and lower
recombination ring 45. The positions at the upper side of the divider
plate are midway between those positions at the lower side of the
divider plate.

10 As most clearly shown in Figure 4 and 5, a pair of
radially-spaced circular channels 60, 64 are cut into the lower surface of
recombination plate 46 and a similar pair of radially spaced circular
channels 70, 74 are cut into the upper surface of recombination plate 45.
15 A plurality of arcuate recombination lands 62 are provided in the lower
surface of recombination plate 46 between channels 60, 64, and a
similar plurality of arcuate recombination lands 72 are provided in the
upper surface of recombination plate 45 between channels 70, 74. Final
20 lands 66, 76 are provided in, respectively, the lower surface of
recombination plate 46 between channel 64 and the inner radial edge of
divider plate of distribution ring 42, and the upper surface of
25 recombination plate 45 between channel 74 and the inner radial edge of
the divider plate. In this embodiment each arcuate land subtends an
area of slightly less than 90°.

coming across recombination land 62a, and also flows radially inwardly across final land 66. The profile (i.e., configuration) of the flow radially inwardly of final land 66 depends largely on the design of the final land, which as discussed hereinafter may be designed with variable lengths and/or gaps to program a desired melt flow profile.

Figure 5a is similar to Figure 5, except that Figure 5a shows the arrangement of the recombination channels and lands at the lower recombination area between the lower surface of divider plate portion and lower recombination ring 45, viewed from above. Although the flow into the lower recombination area is from ports 57, Figure 5a illustrates the arrangement symmetrical about upper port 56a to the upper recombination area so that the relationship between the upper recombination area (of Figure 5) and lower recombination area (of Figure 5a) is most easily appreciated.

In the lower recombination area, flow enters outer recombination channel 70 through lower ports 57d and 57a (shown, and also through lower ports 57b and 57c although not shown in Figure 5a). As in the upper recombination area, the flow from each port flows down outer recombination channel, one half of the flow from each port flowing clockwise and the other half counterclockwise. As described in connection with Figure 5, part of the flow in channel 70 flows radially

inwardly over one of recombination lands 72d and 72a, and the melt
flow remaining at the ends of the lands welds together to form a high
flow weld line 90a, and flows inward through radial recombination
5 channels 71a into inner recombination channel 74. In the inner
recombination the melt flows radially inwardly across final land 76, as
well as in opposite directions down inner recombination channel 74
10 where it is layered under flow coming across recombination lands 72d
and 72a. As in the lower recombination area, final land 76 is designed
with variable lengths and/or gaps to program a desired melt flow profile.

It will be recognized that the recombination lands 62 and land
15 channels 61 of the upper recombination area are offset at 45 degrees
from the lands 72 and channels 71 in the lower recombination area.
This arrangement places high flow weld lines from one recombination
ring radially in line with ports from the opposing recombination ring.
20

Figures 6 and 6a show two preferred melt flow profiles that
exhibit regular division, i.e., the cross sections of the Flows from the
upper and lower recombination areas are identical and fit together with
no intervening space. High flow weld lines 80a and 80b (also 80c and
25 80d) occur in the low flow areas of final land 66. High flow weld lines
90a (also 90b, 90c and 90d) occur in the low flow areas of final land
76. When the upper and lower melt flows join at the inner tip of

divider plate 42d forming combined flow 68, the opposite recombination
rings high final land flow area is added and washes the effects of the
weld lines out. By choosing the shape of the flow profiles 82a, 82b,
5 (82c), 82d, 92a, (92b, 92c) and 92d to be regularly divided, they all
interlock to form a evenly distributed combined flow 68.

The present invention has been described in connection with
10 certain structural embodiments and it will be understood that various
modifications can be made to the above-described embodiments without
departing from the spirit and scope of the invention as defined in the
appended claims.

15 What is claimed is:

20

25

1. In an extrusion die in which material to be extruded flows radially inwardly in the die in a direction generally perpendicular to the central axis of the die and exits the die at an annular orifice in a direction generally parallel to the central axis, said die including a plurality of die layers stacked one upon the other in a direction generally parallel to the central axis, that improvement wherein:
- each of said layers comprises
- an annular flow distribution ring having a radially outer generally cylindrical surface, and
- an annular feed ring surrounding and having a radially inner generally cylindrical surface engaging the outer surface of said flow division ring;
- the feed ring and flow distribution ring of each of said layers include respective surfaces generally perpendicular to the axes thereof and positioned axially above and below the said cylindrical surfaces thereof each of which engages an adjacent surface generally perpendicular to the axis of the die;
- said feed ring includes a flow channel extending generally radially outwardly from the said inner surface of said feed ring and providing for flow of material through said feed ring from said outer surface of said feed ring;

seals are provided between adjacent engaged surfaces to prevent flow from said flow channels of said layers between said engaged surfaces; and,

5

said inner surface of said feed ring and said outer surface of said flow distribution ring define therebetween a series of circumferentially extending channels arranged to divide flow from said flow channel into a plurality of substantially identical flow portions.

10

2. The die of claim 1 wherein said seals are provided between adjacent engaged surfaces generally perpendicular to the axis of said die.

15

3. The die of claim 1 wherein said distribution ring includes a plurality of radially extending flow channels each of which extends from a respective one of said circumferentially extending channels radially inwardly through at least a portion of the radial thickness of said distribution ring and provides for flow of a respective one of said flow portions therethrough.

20

25

4. The die of claim 1 wherein said inner surface of said feed ring and said outer surface of said distribution ring of each layer are

conical and form an angle of less than 30 degrees with the axis of the die.

5

5. The die of claim 1 wherein in each said layer said seals are provided between surfaces of the feed ring thereof perpendicular to the axis of said die and respective surfaces of the distribution ring thereof perpendicular to the axis of said die.

10

6. In an extrusion die in which material exits the die at an annular orifice in a direction generally parallel to the central axis, that improvement comprising:

15

an annular distribution ring arranged to provide for flow of a respective one of a plurality of substantially identical flow portions therethrough,

20

a first subset of said radially extending flow channels of said distribution ring terminating in ports at a first generally axially facing annular surface of said distribution ring,

25

a second subset of said radially extending flow channels of said distribution ring terminating in ports at a second generally axially facing annular surface of said distribution ring, and

said first and second generally axially facing surfaces facing in generally opposite directions.

5

7. The die of claim 6 including a feed ring engaging said distribution ring, said feed ring having a radially inner generally cylindrical surface engaging the outer surface of said flow division ring and including a flow channel extending outwardly from the said inner surface of said feed ring and providing for flow of material through said feed ring to an outer surface of said feed ring, and said inner surface of said feed ring and said outer surface of said flow distribution ring define therebetween a series of circumferentially extending channels arranged to divide flow from said flow channel into said substantially identical flow portions.

20

8. The die of claim 6 including a third generally axially facing surface facing and closely spaced from said first generally axially facing surface and arranged to provide for flow from said first subset generally radially inwardly between said first and third surfaces to an inner annular recombination area, and a fourth generally axially facing surface facing and closely spaced from said second generally axially facing surface and arranged to provide for flow from said second subset

25

generally radially inwardly between said second and fourth surfaces to said recombination area.

5

9. The die of claim 6 wherein

said ports of said first subset are offset circumferentially intermediate said ports of said second subset,

10

a third generally axially facing surface faces and is closely spaced from said first generally axially facing surface thereby providing for flow from said first subset generally radially inwardly between said first and third surfaces to an annular recombination area; and

15

a fourth generally axially facing surface faces and is closely spaced from said second generally axially facing surface thereby providing for flow from said second subset generally radially inwardly between said second and fourth surfaces to said recombination area, and

20

said first, second, third and fourth surfaces are such that said flow between said first and third surfaces and said flow between said second and fourth surfaces are symmetrical and are combined in said recombination area.

25

10. The die of claim 6 including an annular feed ring
surrounding and having a radially inner generally cylindrical surface
engaging an outer surface of said flow distribution ring, and
5 said feed ring including a flow channel extending generally
radially outwardly from the said inner surface of said feed ring and
providing for flow of material through said feed ring from a generally
10 outer surface of said feed ring.

11. In an annular extrusion die in which material exits the die
at an annular orifice in a direction generally parallel to the central axis,
15 a flow recombination system comprising:

an annular ring which provides for flow therethrough to a first
surface; and,

20 a second surface facing and closely spaced from said first surface
and arranged to provide for flow therethrough to spread out from said
ring in generally opposite directions between said first and second
surfaces,

25 said first and second surfaces defining therebetween a region
which provides for greater flow per circumferential portion of the die
than do other flow regions between said first and second surfaces, and

5 said first and second surfaces being arranged such that flows
therebetween in generally opposite directions meet in said region of
greater flow such that a weld between said flows occurs at a region of
relatively high flow and reduces degradation of the flow material.

10 12. The die of claim 11 wherein said first and second
surfaces define therebetween n of said regions of relatively high flow,
said n regions being circumferentially spaced relative to each other at
intervals of about $360/n$ degrees.

15 13. The die of claim 12 wherein said first and second
surfaces are generally axially facing and define therebetween generally
coaxially inner and outer annular flow channels, said material flows
generally inwardly from said outer flow channel to said inner flow
20 channel, and regions between said flow channels define said regions of
relatively high flow and said other regions.

25 14. In an extrusion die in which extruded material exits the
die at an annular orifice in a direction generally parallel to the central
axis, a flow recombination system comprising:

an annular ring arranged to receive a flow and provide for flow thereof through a flow passage of said ring to a first surface; and,

5 a second surface facing and closely spaced from said first surface and arranged to provide for flow from said flow passage between said first and second surfaces,

said first and second surfaces defining therebetween

10 a pair of flow channels, and

a land region between said flow channels, said land region including at least one land, an end of said land being spaced from an adjacent end of a said land to provide for flow therebetween from one of said flow channels to the other of said flow channels, and

15 a surface of said at least one land being spaced from one of said first and second surfaces to provide for flow therebetween from one of said flow channels to the other of said flow channels.

20 15. The die of claim 14 wherein said land region includes a plurality of said lands, and adjacent ends of respective ones of said lands are spaced from each other to provide for flow therebetween from one of said flow channels to the other of said flow channels.

16. The die of claim 14 wherein said annular ring is arranged to receive a plurality of flow portions and includes a plurality of flow passages each of which receives a respective one of said flow portions and provides for flow therethrough to said first surface.

17. The die of claim 16 wherein said flow portions are generally identical.

18. The die of claim 14 wherein said first and second surfaces are generally axially facing and providing for flow from said flow channels radially inwardly between said first and second surfaces.

19. The die of claim 18 wherein said pair of flow channels comprise generally coaxially inner and outer annular flow channels, and said land region is annular and coaxially with and radially between said inner and outer annular flow channels.

20. The die of claim 19 wherein said annular regions includes a plurality of arcuate lands, the adjacent ends of respective ones of the lands being spaced from each other to provide flow therebetween in a

radially inward direction from said outer annular flow channel to said inner annular flow channel.

5

21. The die of claim 18 wherein each of said flow channels in said ring terminates at a respective port at said outer annular flow channel intermediate the length of a respective one of said arcuate lands.

10

22. The die of claim 20 wherein the distances between the adjacent ends of respective ones of said arcuate lands is substantially greater than the gaps between said axially facing surfaces of said lands and said one of said first and second surfaces.

15

23. The die of claim 20 wherein said annular ring includes a second plurality of flow channels each of which receives a respective one of said flow portions and provides for flow therethrough to a third generally axially facing surface; and,

20

a fourth generally axially facing surface facing and closely spaced from said third generally axially facing surface and arranged to provide for flow from said second plurality of flow channels radially inwardly between said third and fourth surfaces,

25

said third and fourth surfaces defining therebetween

second generally coaxial inner and outer annular flow channels,
and

5 a second annular land region coaxial with and radially between
the second inner and outer annular flow channels,

the second annular land region including a plurality of arcuate
lands, the adjacent ends of respective ones of the lands of the second
10 annular region being spaced from each other to provide for flow
therebetween in a radially inward direction from said second outer
annular flow channel to said second inner annular flow channel, and

a generally axially facing surface of each of said land of the
15 second annular region being spaced from one of said third and fourth
surfaces to provide for flow therebetween in a radially inward direction
from said second outer annular flow channel to said second inner
annular flow channel.

20

24. The die of claim 23 wherein the first and third generally
axially facing surfaces face in generally opposite directions, and
25 including a recombination region in which the flow between said first
and second surfaces is combined with the flow between said third and
fourth surface.

25. The die of claim 24 including a third annular land region spaced from one of said first and second surfaces to provide a flow gap therebetween for flow in a radially inward direction from between said
5 first and second surfaces to said recombination area, and a fourth annular land region spaced from one of said third and fourth surfaces to provide a flow gap therebetween for flow in a radially inward direction
10 from between said third and fourth surfaces to said recombination area.

26. In an extrusion die in which material exits the die at an annular orifice in a direction generally parallel to the central axis:

15 a flow ring having at least one flow passage which extends radially inwardly through at least a portion of the radial thickness of said ring and provides for flow therethrough,

20 said at least one flow passage terminating in a first subset of a circumferentially spaced ports at a first generally axially facing annular surface of said flow ring and in a second subset of circumferentially spaced ports at a second generally axially facing annular surface of said
25 flow ring,

said first and second generally axially facing surfaces facing in generally opposite directions,

5 a third generally axially facing surface facing and closely spaced from said first generally axially facing surface and arranged to provide for flow from said first subset generally radially inwardly between said first and third surfaces; and

10 a fourth generally axially facing surface facing and closely spaced from said second generally axially facing surface and arranged to provide for flow from said second subset generally radially inwardly between said second and fourth surfaces,

15 said first and third surfaces defining therebetween a first annular land region,

said second and fourth surfaces defining therebetween a second annular land region,

20 said first annular land region including a first flow gap therebetween, and

said second annular region including a second flow gap therebetween.

25 27. The die of claim 26 wherein said flow ring includes a plurality of flow channels extending radially through at least a portion of the radial thickness of said ring and providing for flow therethrough, a first subset of said radially extending flow channels terminating in

5 respective ones of said first set of circumferentially spaced ports and a
second subset of said radially extending flow channels terminating in
respective ones of said second set of circumferentially spaced ports.

10 28. The die of claim 26 wherein said first and third surfaces
define therebetween a first generally coaxial annular flow channel and
said first annular region is coaxial with and radially within the first
annular flow channel, and said second and fourth surfaces define
therebetween a second generally coaxial annular flow channel and said
15 second annular land region is coaxial with and radially within the first
annular flow channel.

20 29. The die of claim 28 wherein said first annular land region
includes a surface spaced from one of said first and third surfaces to
provide said first flow gap for flow from said first flow channel, and
said second annular land region includes a surface spaced from one of
said second and fourth surfaces to provide said second flow gap for
25 flow from said second flow channel.

5 30. The die of claim 29 wherein the said surfaces defining
said first and second flow gaps are generally axially facing and the
flows in said gaps are in a generally radially inwardly direction.

10 31. The die of claim 26 wherein said ports of said first set
are offset circumferentially intermediate said ports of said second set.

15 32. The die of claim 26 wherein said first gap and said
second gap are symmetrical and circumferentially offset relative to each
other.

20 33. The die of claim 26 wherein said first gap and said
second gap are arranged such that the flow through one of said gaps has
a cross section identical to that of the flow through the other of said
gaps, and said cross-sections are such that said flows join together
inwardly of said gap to create a uniform combined flow.

25 34. In an extrusion die in which material exits the die at an
annular orifice in a direction generally parallel to the central axis, that
improvement comprising:

a flow ring having generally opposed first and second surfaces
and providing for flow to each of said first and second surfaces,

5 a third surface facing and closely spaced from said first surface
and arranged to provide for a first flow therebetween such that said first
flow includes a first weld region of relatively low flow and regions of
relatively higher flow adjacent thereto,

10 a fourth surface facing and closely spaced from said second
surface and arranged to provide for a second flow from said second
subset therebetween such that said second flow therebetween includes a
second weld region of relatively low flow and regions of relatively
15 higher flow adjacent thereto,

said first, second, third and fourth surfaces being such that said
first weld region is offset relative to said second weld region and being
arranged such that said first flow is joined with said second region with
20 said first weld region of said first flow adjacent a said region of
relatively higher flow of said second flow and with said second weld
region of said second flow adjacent a said region of relatively higher
25 flow of said first flow.

5 35. The die of claim 34 wherein said flow distribution ring has a plurality of flow passages each of which extends through at least a portion of the ring, is arranged to provide for flow of a flow portion therethrough, and terminates at a port at a respective one of said first and second surfaces.

10 36. The die of claim 35 wherein said ports include a first set of circumferentially spaced ports at said first surface and a second set of circumferentially spaced ports at said second surface, said ports at said first surface being circumferentially intermediate said ports at said first surface.

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FIG. 5

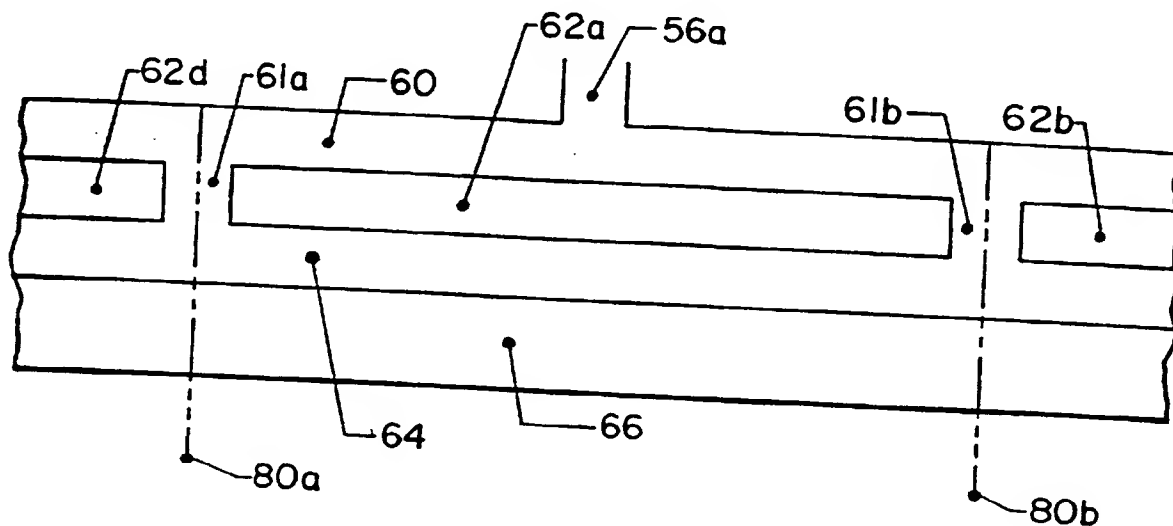
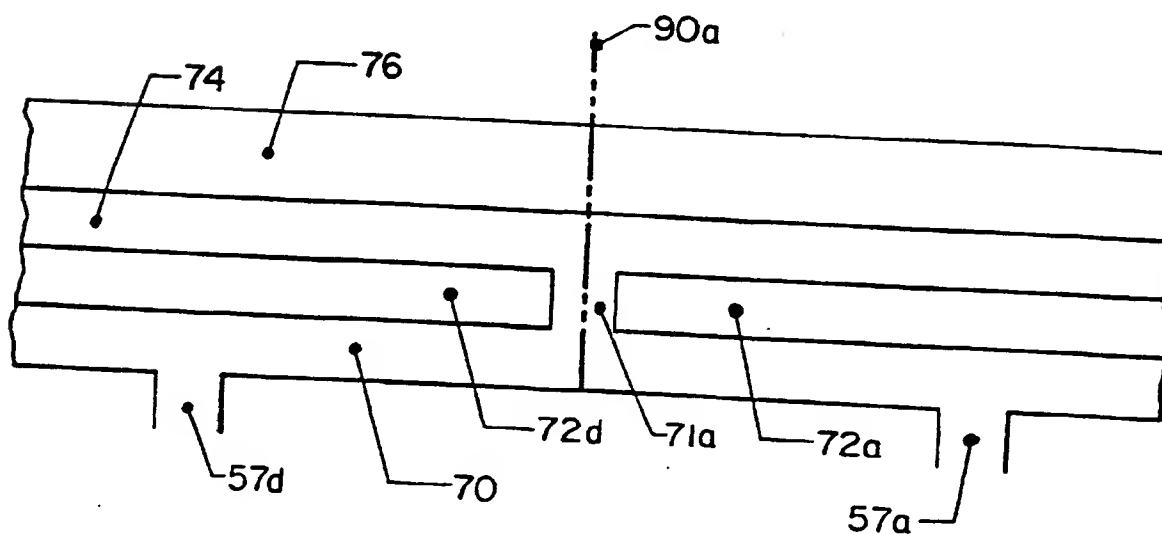


FIG. 5a



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Fig. 6

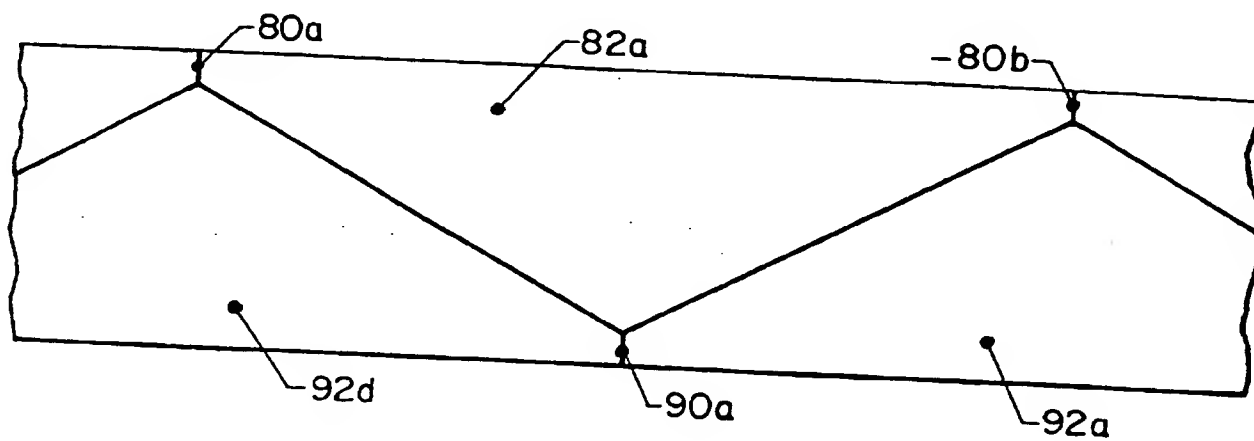
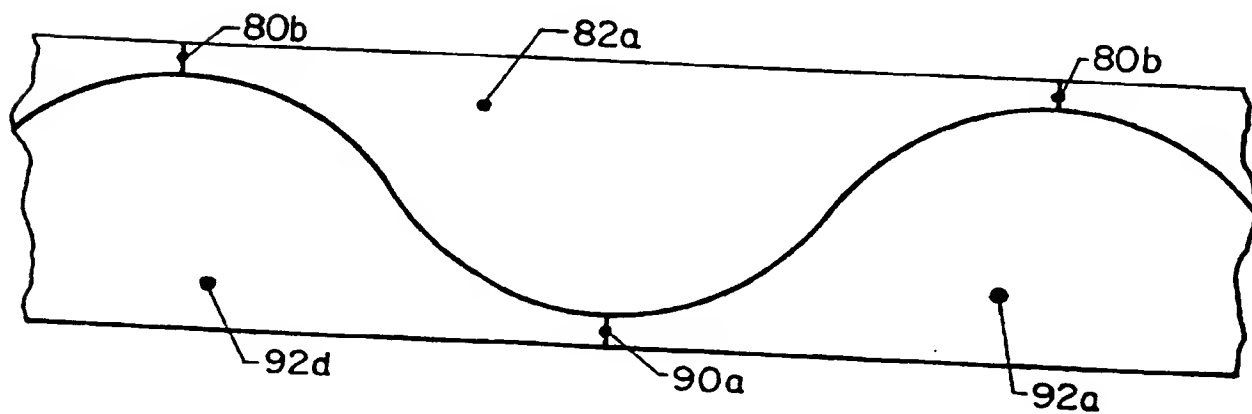


Fig. 6a



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INTERNATIONAL SEARCH REPORT

Int. Application No.
PCT/US 97/14952

A. CLASSIFICATION OF SUBJECT MATTER
IPC 6 B29C47/28 B29C47/70

According to International Patent Classification (IPC) or to both national classification and IPC

B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)
IPC 6 B29C

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practical, search terms used)

C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
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Y		1-5, 8, 9, 11-36
Y	EP 0 252 388 A (GEN ELECTRIC ; GRAHAM ENG CORP (US)) 13 January 1988 see abstract see page 5, line 25 - line 30 see figures 1, 2	1-5
Y	WO 89 00910 A (KIRJAVAINEN KARI) 9 February 1989 see abstract see page 4, line 29 - page 5, line 4 see figures 1, 8	8, 9, 11-36
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☒ Further documents are listed in the continuation of box C.

☒ Patent family members are listed in annex.

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Date of the actual completion of the international search

20 November 1997

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Name and mailing address of the ISA

European Patent Office, P.B. 5818 Patentlaan 2
NL - 2280 HV Rijswijk
Tel. (+31-70) 340-2040, Tx. 31 651 epo nl.
Fax: (+31-70) 340-3016

Authorized officer

Jensen, K

INTERNATIONAL SEARCH REPORT

International Application No

PCT/US 97/14952

C. (Continuation) DOCUMENTS CONSIDERED TO BE RELEVANT

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A	DE 90 03 537 U (ERICH BECK) 7 June 1990 see the whole document ----	1,6,11, 14,26,34
A	DE 42 18 095 A (REIFENHAEUSER MASCH) 9 December 1993 see abstract see figures ----	1-7, 10-13
A	FR 2 308 490 A (BONNEL PIERRE) 19 November 1976 see figures -----	1-7, 10-13

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